



NUMERICAL APPROACH OF HEAT AND MASS TRANSFER OF MHD CASSON FLUID UNDER RADIATION OVER AN EXPONENTIALLY PERMEABLE STRETCHING SHEET WITH CHEMICAL REACTION AND HALL EFFECT

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ABSTRACT

In this paper, heat and mass transfer of MHD Casson fluid under radiation over an exponentially permeable stretching sheet with chemical reaction and Hall Effect investigated numerically. Suitable similarity transformations are used to convert the governing partial differential equations to nonlinear ordinary differential equations. Using a numerical technique named Keller box method the equations are then solved. Study of various effects such as chemical reaction, hall effect, suction /injection on magneto hydrodynamic Casson fluid along with radiation the heat source parameter, chemical reaction parameter, Schmidt number are tabulated for various parameters. Also local parameters are calculated and compared with previous literature the results are found to be in good agreement. The velocity, temperature, concentration visual representations are plotted for various parameters using matlab. Skin friction coefficient, Nusselt number and Sherwood number are calculated in both cases of Newtonian and non-Newtonian it is observed that the friction factor and the heat and mass transfer rates reduces for increase in magnetic parameter. Also for progressive values of radiation parameter, thermal grashof number, concentration grashof number and hall parameter, skin friction coefficient, heat and mass transfer rates increases where as they decreases for chemical reaction parameter, Schmidt number.

Keywords: MHD, Casson fluid, Chemical reaction, radiation, Hall Effect.

1. INTRODUCTION

Experience shows that due to several industrial applications of Non Newtonian fluids such as polymer industry and mining industry attracted many researchers to study about non Newtonian fluids. Also fluid flow over a stretching sheet is extensively used in manufacturing process because there is an association between stretching sheet and fluid that flows on it.

Dutta *et al.* (1985) analyzed fluid flow on a stretching sheet with uniform heat flux and observed that with increase in Prandtl number first wall temperature increases quickly and then decreases gradually. Masahide and Tadashi (1988) proved that with the non-Newtonian property of blood, flow speed decreases along the stenosis. James and Milivoje (1990a) provided theoretical and practical study of heat transfer effects in both the cases of Newtonian and Non Newtonian fluid. Lai (1990b) derived a closed form of solutions for a special case of Lewis number. Lin and Wu (1995) studied boundary layer flow in case of a vertical plate and the effects of buoyancy ratio and Lewis number on Heat and mass transfer are observed. Magyari and Keller (1999) observed that boundary layer thickness increases on enhancing the value of wall temperature distribution by fixing Prandtl number also by keeping wall temperature fixed and enhancing Prandtl number. Swathi Mukhopadhyay *et al.* (2005) observed that by expanding the length of the stretching sheet velocity of the fluid decreases by reducing thickness of the fluid. Later, Subhas *et al.* (2010) analyzed non Newtonian fluid flow through a porous medium along with the effect of suction concluded that wall temperature will be decreased with the effect of viscous dissipation. Vedavathi *et al.* (2015) used Runge-Kutta fourth order and concluded that suction effect maintains fixed growth of the thermal, concentration, hydrodynamic boundary layers. After that Vedavathi *et al.* (2017) concluded that on increasing radiation absorption parameter velocity profiles will be enhanced and increasing Prandtl number skin friction number decreases.

Talla, Kumari and Sridhar (2018a) studied MHD Casson fluid flow over a exponentially stretching surface and observed that with increase in Casson parameter velocity reduces and concentration increases. Reddy and Krishna (2018b) observed that as the Soret number increases velocity boundary layer, thermal boundary layer, concentration boundary layer diminishes. Chandra Sekhar (2018c) observed that temperature increases with increase of chemical reaction parameter. Konda Reddy *et al.* (2018d) studied MHD mixed convection flow of a Casson Nano fluid over a nonlinear stretching sheet temperature, concentration enhanced and velocity diminished with increase in Casson parameter. Charan Kumar *et al.* (2018e) used RK- Fehlberg method to study the effects of joule heating and chemical reaction effects on fluid flow over a stretching sheet along with radiation and porous medium. Anki Reddy and Suneetha (2018f) concluded that temperature of the fluid and thermal relaxation time are oppositely related. Ghiasi and Saleh (2018g) witnessed that casson fluid along with suction effect reduces heat, mass transfer rates. Flihi *et al.* (2019a) concluded that fluid temperature raises with increase in dissipation parameter. Dharmiah *et al.* (2019b) used perturbation method and observed that chemical reaction parameter dominates the concentration profiles. Sampath and Pai (2019c) found that enhancing magnetic parameter skin friction decreases. Nagaraju *et al.* (2019d) used HAM technique and concluded that raise in magnetic parameter enhances velocity also energy dissipation step ups causing increase in temperature, later Huang pin *et al.* (2019e) used Keller box method and observed that suction increases the Nusselt number and Sherwood number. Blowing reduces them. Ganapathirao *et al.* (2019f) found that skin friction and coefficient of heat transfer raises with enhancing buoyancy parameter. Ibrahim *et al.* (2019g) observed that velocity increases with increasing buoyancy parameter. Raghunandana Sai and Ramana Murthy (2019h) studied the impact of various parameters on velocity and temperature profiles and observed that with increase in Prandtl number and time temperature increases. Ravi Kumar *et al.* (2019i) noticed that with

increase in slip parameter, Grashof's number velocity increases. Kavitha and Naikoti (2019j) used quasi-linearization technique to study the power law fluid flow under the influence of radiation. Swamy *et al.* (2019k) studied MHD flow in a porous channel with suction and observed that as the intensity of the magnetic field increases fluid velocity reduces. Vijaya and Reddy (2019l) analyzed the MHD Casson fluid flow on a vertical porous plate using Perturbation technique method. Manjula and Chandra Sekhar (2019m) observed Soret and heat generation effects on Casson fluid flow concluded that raise in Soret number values increases buoyancy force hence velocity increases. Sivaiah *et al.* (2019n) concluded that due to thermal radiation parameter, temperature decreases and with the presence of Eckert number temperature increases. Dharmiah. *et al.* (2019o) implemented perturbation technique and noticed that concentration of the fluid reduces with the presence of chemical reaction. Balamurugan *et al.* (2020a) concluded that entropy generation increases for higher values of magnetic parameter or thermal radiation parameter. Later Vijaya *et al.* (2020b) used bvp4c technique and noted that for increasing values of magnetic parameter velocity of fluid improved. Dharmiah. *et al.* (2020c) studied the influence of hall and ion slip on a Nano fluid and concluded that skin friction coefficient raises with magnetic parameter. Nagalakshmi and vijaya(2020d) used Runge Kutta method and observes for progressive values of Prandtl number thermal boundary layer thickness diminishes. Ibrahim. *et al.* (2020e) used Homotopy analysis method to study the influence of various parameters like radiation, chemical reaction of MHD casson fluid flow over a stretching sheet.

The study of flow above an exponentially stretching sheet has significant applications in various industries and technological processes for example fluid film condensation process, cooling process of metallic sheets, design of chemical processing equipment, polymer industries. Also the radiation effect on MHD boundary layer flow has various applications in manufacturing industries like glass-fiber production, paper production etc. Hall effect has some industrial applications like automotive safety, fluid monitoring, building automation, personal electronics like disk drives, power supply protectors .with this interest in the present paper, Keller Box method was implemented to study the influence of hall effect in presence of radiation and chemical reaction of MHD Casson fluid flow on an exponentially permeable stretching sheet.

2. FORMULATION OF THE PROBLEM

In this study a steady, two dimensional, incompressible, radiative, MHD Casson fluid flow over an exponentially permeable stretching sheet under the influence of Hall Effect is considered. u, v represents velocity components in x and y directions. The exponentially stretching sheet is assumed to be at $y=0$. Also flow is assumed to be above x -axis only. Magnetic field is applied externally normal to stretching sheet. The magnetic Reynolds number is very small because of the magnetic field. Here we used external heat source, Hall Effect, chemical reaction.

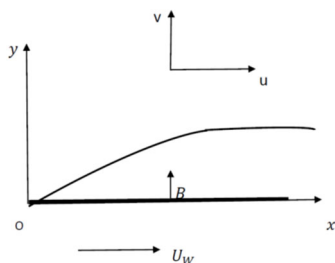


Fig. 1 Flow model of the problem

The rheological equation of Casson fluid is

$$\tau_{ij} = \begin{cases} 2(\mu_B + p_y * (2\pi)^{-0.5})e_{ij}, \pi > \pi_c \\ 2(\mu_B + p_y * (2\pi_c)^{-0.5})e_{ij}, \pi < \pi_c \end{cases}$$

Where μ_B is plastic dynamic viscosity, P_y is yield stress, π is (i, j) th component of deformation rate, π_c is critical value of this product.

Supporting to the above assumptions the guiding partial differential equations are taken as below.

$$u_x + v_y = 0 \tag{1}$$

$$uu_x + vv_y = \nu(1 + \frac{1}{\beta})u_{xx} + g\beta_T(T - T_\infty) + g\beta_C(C - C_\infty) - \frac{\sigma B^2 u}{\rho(1+m^2)} \tag{2}$$

$$uT_x + vT_y = \frac{k}{\rho C_p}T_{yy} + \frac{\nu}{C_p}(1 + \frac{1}{\beta})u_y^2 - \frac{1}{\rho C_p}Q_0(T - T_\infty) + \frac{\sigma B^2 u^2}{\rho(1+m^2)} - \frac{1}{\rho C_p}(q_r)_y \tag{3}$$

$$uC_x + vC_y = D_m C_{yy} - k_1(C - C_\infty) \tag{4}$$

Boundary conditions are

$$\left. \begin{aligned} u &= U, & u &\rightarrow 0, \\ v &= -V(x), \text{ at } y = 0 \ \& \ T \rightarrow T_\infty, \text{ as } y \rightarrow \infty \\ T &= T_w, & C &\rightarrow C_\infty \\ C &= C_w \end{aligned} \right\} \tag{5}$$

By observing the equations here we introduce the similarity transformations,

$$\left. \begin{aligned} u &= U_0 e^{\frac{Nx}{L}} f'(\eta) \\ v &= -\sqrt{\frac{U_0 \nu}{2L}} e^{\frac{Nx}{2L}} N(f(\eta) + \eta f'(\eta)) \\ \psi &= \sqrt{2U_0 \nu L} e^{\frac{Nx}{2L}} f(\eta) \\ T &= T_\infty + T_0 e^{\frac{2Nx}{L}} \theta(\eta) \\ C &= C_\infty + C_0 e^{\frac{2Nx}{L}} \phi(\eta) \\ \eta &= y \sqrt{\frac{U_0}{2\nu L}} e^{\frac{Nx}{2L}} \end{aligned} \right\} \tag{6}$$

The partial differential equations are transformed to

$$\left(1 + \frac{1}{\beta}\right) \frac{d^3 f}{d\eta^3} + N \left[f \frac{d^2 f}{d\eta^2} - 2 \left(\frac{df}{d\eta} \right)^2 \right] + 2Gr\theta + 2Gc\phi - \frac{Ha^2}{1+m^2} \frac{df}{d\eta} = 0 \tag{7}$$

$$\left(1 + \frac{4}{3}R\right) \frac{d^2 \theta}{d\eta^2} + Pr N \left[f \frac{d\theta}{d\eta} - 4 \frac{df}{d\eta} \theta \right] + \left(1 + \frac{1}{\beta}\right) Pr Ec \frac{d^2 f}{d\eta^2} - Pr Q\theta + \frac{Pr J}{1+m^2} \frac{d^2 f}{d\eta^2} = 0 \tag{8}$$

$$\frac{d^2 \phi}{d\eta^2} + Sc \left[f \frac{d\phi}{d\eta} - 4 \frac{df}{d\eta} \phi \right] - Sc \gamma \phi = 0 \tag{9}$$

$$\left. \begin{aligned} &f = S, f' = 1 && \text{at } \eta = 0 \\ &\theta = 1, \phi = 1 \\ &f' = 0 && \text{at } \eta \rightarrow \infty \\ &\theta = 0, \phi = 0 \end{aligned} \right\} \quad (10)$$

3. NUMERICAL PROCEDURE

The moderate implicit finite difference method called Keller Box method to convert equations (7)-(9) into first order. By using this method, the resultant equations are linearized and then converted into matrix form by introducing Newton's method. Finally, the tri-diagonal elimination method is applied to solve the linear system of equations Cebeci *et al.* (1988).

$$\left. \begin{aligned} &\text{Introducing } f' = p, p' = q \\ &g = \theta, g' = t \\ &s = \phi, s' = n \end{aligned} \right\} \quad (11)$$

The equations (7), (8), (9) are transformed to

$$\left(1 + \frac{1}{\beta}\right)q' + N[fq - 2p^2] + 2Grg + 2Gcs - \frac{Ha^2}{1+m^2}p = 0 \quad (12)$$

$$\left(1 + \frac{4R}{3}\right)t' + Pr N[ft - 4pg] + \left(1 + \frac{1}{\beta}\right)Pr Ecq^2 - Pr Qg + \frac{Pr J}{1+m^2}p^2 = 0 \quad (13)$$

$$n' + Sc[fn - 4ps] - Sc\gamma s = 0 \quad (14)$$

Using finite differences

$$\left. \begin{aligned} f_j - f_{j-1} &= h_j \left(\frac{p_j + p_{j-1}}{2}\right) \\ p_j - p_{j-1} &= h_j \left(\frac{q_j + q_{j-1}}{2}\right) \\ g_j - g_{j-1} &= h_j \left(\frac{t_j + t_{j-1}}{2}\right) \\ s_j - s_{j-1} &= h_j \left(\frac{n_j + n_{j-1}}{2}\right) \\ \left(1 + \frac{1}{\beta}\right) &\left[\left(\frac{q_j - q_{j-1}}{h_j}\right) + \right. \\ &N\left[\left(\frac{f_j + f_{j-1}}{2}\right)\left(\frac{q_j + q_{j-1}}{2}\right) - 2\left(\frac{p_j + p_{j-1}}{2}\right)^2\right] + 2Gr\left(\frac{g_j + g_{j-1}}{2}\right) + 2Gc\left(\frac{s_j + s_{j-1}}{2}\right) \\ &\left. - \frac{Ha^2}{1+m^2}\left(\frac{p_j + p_{j-1}}{2}\right)\right] = 0 \\ \left(1 + \frac{4R}{3}\right) &\left[\left(\frac{t_j - t_{j-1}}{h_j}\right) + \right. \\ &Pr N\left[\left(\frac{f_j + f_{j-1}}{2}\right)\left(\frac{t_j + t_{j-1}}{2}\right) - 4\left(\frac{p_j + p_{j-1}}{2}\right)\left(\frac{g_j + g_{j-1}}{2}\right)\right] \\ &+ \left(1 + \frac{1}{\beta}\right)Pr Ec\left(\frac{q_j + q_{j-1}}{2}\right)^2 \\ &\left. - Pr Q\left(\frac{g_j + g_{j-1}}{2}\right) + \frac{Pr J}{1+m^2}\left(\frac{p_j + p_{j-1}}{2}\right)^2\right] = 0 \end{aligned} \right\} \quad (15)$$

$$\left. \begin{aligned} &\left(\frac{n_j + n_{j-1}}{h_j}\right) + \\ &Sc\left[\left(\frac{f_j + f_{j-1}}{2}\right)\left(\frac{n_j + n_{j-1}}{2}\right) - 4\left(\frac{p_j + p_{j-1}}{2}\right)\left(\frac{s_j + s_{j-1}}{2}\right)\right] \\ &- Sc\gamma\left(\frac{s_j + s_{j-1}}{2}\right) = 0 \end{aligned} \right\}$$

We linearize the system of equations given in (15) Using Newton's method for that we introduce

$$\left. \begin{aligned} f_j^{k+1} &= f_j^k + \delta f_j^k \\ p_j^{k+1} &= p_j^k + \delta p_j^k \\ q_j^{k+1} &= q_j^k + \delta q_j^k \\ g_j^{k+1} &= g_j^k + \delta g_j^k \\ t_j^{k+1} &= t_j^k + \delta t_j^k \\ s_j^{k+1} &= s_j^k + \delta s_j^k \\ n_j^{k+1} &= n_j^k + \delta n_j^k \end{aligned} \right\} \quad (16)$$

Substitute them in above system (15) we get the system of equations as

$$\left. \begin{aligned} \delta f_j - \delta f_{j-1} - \frac{h_j}{2}(\delta p_j + \delta p_{j-1}) &= (r_1)_j \\ \delta p_j - \delta p_{j-1} - \frac{h_j}{2}(\delta q_j + \delta q_{j-1}) &= (r_2)_j \\ \delta g_j - \delta g_{j-1} - \frac{h_j}{2}(\delta t_j + \delta t_{j-1}) &= (r_3)_j \\ \delta s_j - \delta s_{j-1} - \frac{h_j}{2}(\delta n_j + \delta n_{j-1}) &= (r_4)_j \\ (a_1)_j \delta q_j + (a_2)_j \delta q_{j-1} + (a_3)_j \delta f_j + (a_4)_j \delta f_{j-1} \\ + (a_5)_j \delta p_j + (a_6)_j \delta p_{j-1} + (a_7)_j \delta g_j + (a_8)_j \delta g_{j-1} \\ + (a_9)_j \delta s_j + (a_{10})_j \delta s_{j-1} &= (r_5)_j \\ (b_1)_j \delta t_j + (b_2)_j \delta t_{j-1} + (b_3)_j \delta f_j + (b_4)_j \delta f_{j-1} + (b_5)_j \delta g_j + \\ (b_6)_j \delta g_{j-1} + (b_7)_j \delta q_j + (b_8)_j \delta q_{j-1} &= (r_6)_j \\ (c_1)_j \delta n_j + (c_2)_j \delta n_{j-1} + (c_3)_j \delta f_j + (c_4)_j \delta f_{j-1} + (c_5)_j \delta s_j \\ + (c_6)_j \delta s_{j-1} + (c_7)_j \delta p_j + (c_8)_j \delta p_{j-1} &= (r_7)_j \end{aligned} \right\} \quad (17)$$

Where j=1, 2, 3

$$\left. \begin{aligned} (r_1)_j &= f_{j-1} - f_j + \frac{h_j}{2}(p_j + p_{j-1}) \\ (r_2)_j &= p_{j-1} - p_j + \frac{h_j}{2}(q_j + q_{j-1}) \\ (r_3)_j &= g_{j-1} - g_j + \frac{h_j}{2}(t_j + t_{j-1}) \\ (r_4)_j &= s_{j-1} - s_j + \frac{h_j}{2}(n_j + n_{j-1}) \end{aligned} \right\} \quad (18)$$

$$(r_5)_j = q_{j-1} - q_j - \frac{N\beta h_j}{4(\beta + 1)}(f_j + f_{j-1})(q_j + q_{j-1}) + \frac{N\beta h_j}{2(\beta + 1)}(p_j + p_{j-1})^2 - \frac{Gr\beta h_j}{\beta + 1}(g_j + g_{j-1}) - \frac{Gc\beta h_j}{\beta + 1}(s_j + s_{j-1}) + \frac{Ha^2 \beta h_j}{2(\beta + 1)(1 + m^2)}(p_j + p_{j-1})$$

$$(r_6)_j = t_{j-1} - t_j - \frac{3Pr N}{4(3 + 4R)}(f_j + f_{j-1})(t_j + t_{j-1})$$

$$+ \frac{3Pr N}{3 + 4R}(p_j + p_{j-1})(g_j + g_{j-1})$$

$$- \frac{\beta + 1}{\beta} \frac{3Pr Ech_j}{4(3 + 4R)}(q_j + q_{j-1})^2$$

$$+ \frac{3Pr Q}{2(3 + 4R)}(g_j + g_{j-1})$$

$$- \frac{3Pr h_j J}{4(3 + 4R)(1 + m^2)}(p_j + p_{j-1})^2$$

$$(r_7)_j = n_{j-1} - n_j - \frac{Sch_j}{4}(f_j + f_{j-1})(n_j + n_{j-1})$$

$$+ Sch_j(p_j + p_{j-1})(s_j + s_{j-1}) + \frac{Sc\gamma h_j}{2}(s_j + s_{j-1})$$

$$(a_2)_j = (a_1)_j - 2.0$$

$$(a_3)_j = \frac{N\beta h_j}{4(\beta + 1)}(q_j + q_{j-1})$$

$$(a_4)_j = (a_3)_j$$

$$(a_5)_j = -\frac{N\beta h_j}{\beta + 1}(p_j + p_{j-1}) - \frac{Ha^2 \beta h_j}{2(\beta + 1)(1 + m^2)}(p_j + p_{j-1})$$

$$(a_6)_j = (a_5)_j \tag{19}$$

$$(a_7)_j = \frac{Gr\beta h_j}{\beta + 1},$$

$$(a_8)_j = (a_7)_j$$

$$(a_9)_j = \frac{Gc\beta h_j}{\beta + 1},$$

$$(a_{10})_j = (a_9)_j$$

$$(b_1)_j = 1 + \frac{3Pr Nh_j}{4(3 + 4R)}(f_j + f_{j-1})$$

$$(b_2)_j = (b_1)_j - 2.0$$

$$(b_3)_j = \frac{3Pr Nh_j}{4(3 + 4R)}(t_j + t_{j-1}) \tag{20}$$

$$(b_4)_j = (b_3)_j$$

$$(b_5)_j = \frac{-3Pr Nh_j}{3 + 4R}(p_j + p_{j-1}) - \frac{3Pr Qh_j}{2(3 + 4R)}$$

$$(b_6)_j = (b_5)_j$$

$$(b_7)_j = -\frac{3Pr Nh_j}{(3 + 4R)}(g_j + g_{j-1}) +$$

$$\frac{3Pr h_j J}{2(3 + 4R)(1 + m^2)}(p_j + p_{j-1})$$

$$(b_8)_j = (b_7)_j$$

$$(b_9)_j = \frac{3}{2} \left(\frac{\beta + 1}{\beta} \right) \frac{Pr Ech_j}{(3 + 4R)}(q_j + q_{j-1})$$

$$(b_{10})_j = (b_9)_j$$

$$(c_1)_j = 1 + \frac{Sch_j}{4}(f_j + f_{j-1})$$

$$(c_2)_j = (c_1)_j - 2.0$$

$$(c_3)_j = \frac{Sch_j}{4}(n_j + n_{j-1})$$

$$(c_4)_j = (c_3)_j \tag{21}$$

$$(c_5)_j = -Sch_j(p_j + p_{j-1}) - \frac{Sc\gamma h_j}{2}$$

$$(c_6)_j = (c_5)_j$$

$$(c_7)_j = -Sch_j(s_j + s_{j-1})$$

$$(c_8)_j = (c_7)_j$$

For $j=1, 2, 3, \dots$

The system of equations become

$$[A_1][\delta_1] + [C_1][\delta_2] = [r_1] \tag{22}$$

$$[B_2][\delta_1] + [A_2][\delta_2] + [C_2][\delta_3] = [r_2]$$

.....

$$[B_{j-1}][\delta_1] + [A_{j-1}][\delta_2] + [C_{j-1}][\delta_3] = [r_{j-1}]$$

$$[B_j][\delta_{j-1}] + [A_j][\delta_j] = [r_j]$$

Where,

$$A_1 = \begin{bmatrix} 0 & 0 & 0 & 1 & 0 & 0 & 0 \\ d & 0 & 0 & 0 & d & 0 & 0 \\ 0 & d & 0 & 0 & 0 & d & 0 \\ 0 & 0 & -1 & 0 & 0 & 0 & d \\ (a_2)_1 & 0 & (a_{10})_1 & (a_3)_1 & (a_1)_1 & 0 & 0 \\ (b_{10})_1 & (b_2)_1 & 0 & (b_3)_1 & (b_9)_1 & (b_1)_1 & 0 \\ 0 & 0 & (c_6)_1 & (c_3)_1 & 0 & 0 & (c_1)_1 \end{bmatrix}$$

$$A_j = \begin{bmatrix} d & 0 & 0 & 1 & 0 & 0 & 0 \\ -1 & 0 & 0 & 0 & d & 0 & 0 \\ 0 & -1 & 0 & 0 & 0 & d & 0 \\ 0 & 0 & -1 & 0 & 0 & 0 & d \\ (a_6)_2 & (a_8)_2 & (a_{10})_2 & (a_3)_2 & (a_1)_2 & 0 & 0 \\ (b_8)_2 & (b_6)_2 & 0 & (b_3)_2 & (b_9)_2 & (b_1)_2 & 0 \\ (c_8)_2 & 0 & (c_6)_2 & (c_3)_2 & 0 & 0 & (c_1)_2 \end{bmatrix}$$

Where $j=2, 3, n-1$

$$B_j = \begin{bmatrix} 0 & 0 & 0 & -1 & 0 & 0 & 0 \\ 0 & 0 & 0 & 0 & d & 0 & 0 \\ 0 & 0 & 0 & 0 & 0 & d & 0 \\ 0 & 0 & 0 & 0 & 0 & 0 & d \\ 0 & 0 & 0 & (a_4)_2 & (a_2)_2 & 0 & 0 \\ 0 & 0 & 0 & (b_4)_2 & (b_{10})_2 & (b_2)_2 & 0 \\ 0 & 0 & 0 & (c_4)_2 & 0 & 0 & (c_2)_2 \end{bmatrix} \text{ and}$$

$$C_j = \begin{bmatrix} d & 0 & 0 & 0 & 0 & 0 & 0 \\ 1 & 0 & 0 & 0 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 & 0 & 0 & 0 \\ 0 & 0 & 1 & 0 & 0 & 0 & 0 \\ (a_5)_2 & (a_7)_2 & (a_9)_2 & 0 & 0 & 0 & 0 \\ (b_7)_2 & (b_5)_2 & 0 & 0 & 0 & 0 & 0 \\ (c_7)_2 & 0 & (c_5)_2 & 0 & 0 & 0 & 0 \end{bmatrix}$$

Where $j=1, 2, 3, n-1$.

The resultant linear equations are solved by LU decomposition method, the process of calculation should be terminated until it satisfies convergence criteria. The calculations are terminated for $|\delta g_0^{(i)}| < \epsilon$

where $\epsilon = 0.000001$.

4. RESULTS AND DISCUSSION

Graphs are plotted for various parameters like Hartman's number, exponential parameter, Thermal Grashof's number, concentration Grashof's number, radiation parameter, Prandtl number, heat source parameter, Eckert number, Schmidt number, chemical reaction parameter, Suction parameter, Hall parameter using MATLAB.

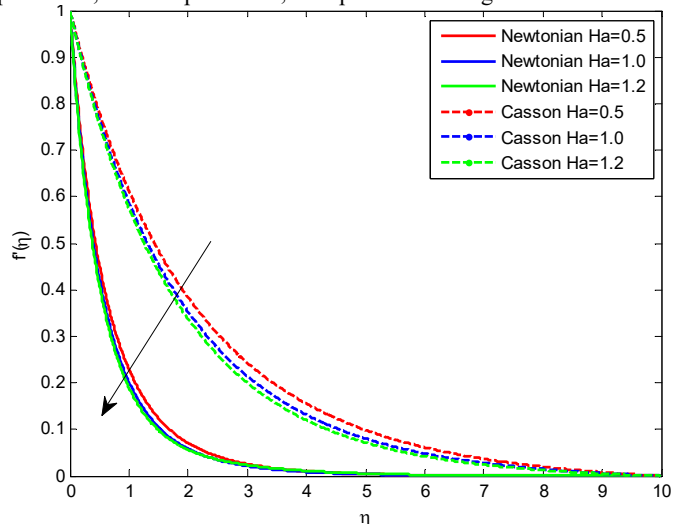


Fig. 2 Effect of Ha on Velocity

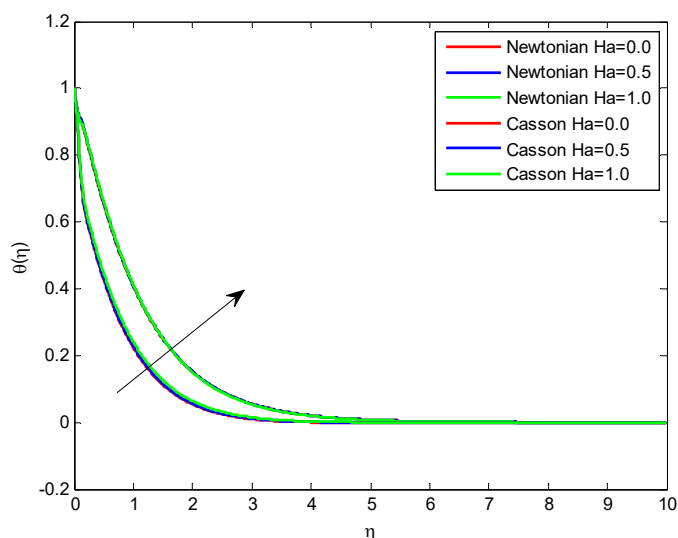


Fig. 3 Effect of Ha on Temperature

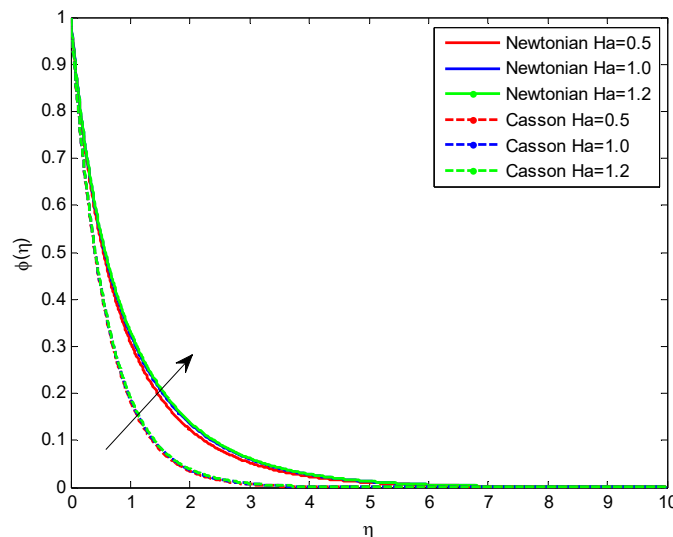


Fig. 4 Effect of Ha on concentration

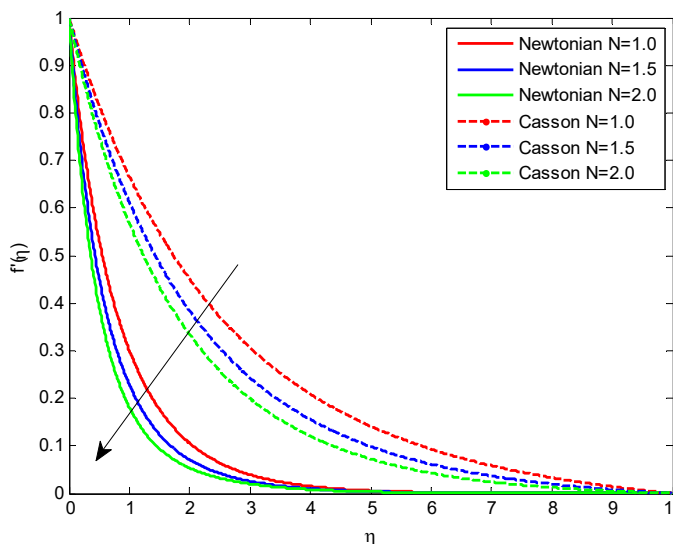


Fig. 5 Effect of N on Velocity

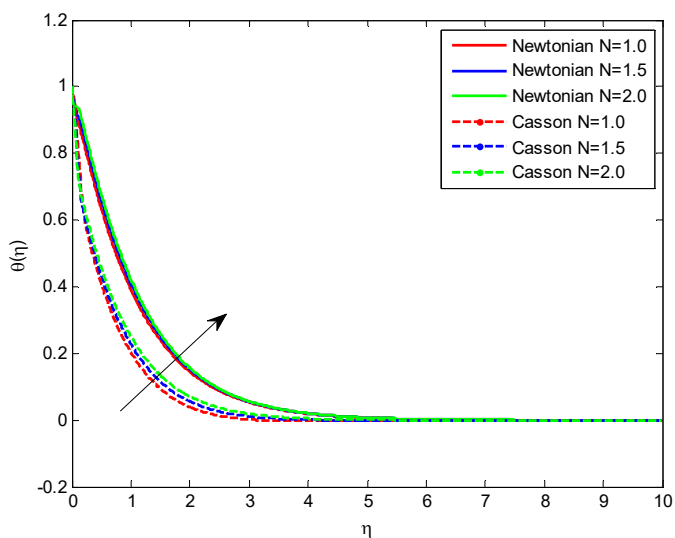


Fig. 6 Effect of N on Temperature

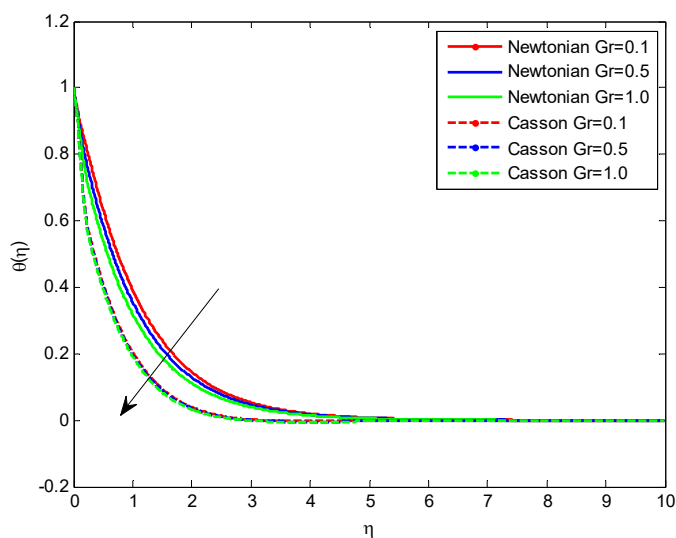


Fig. 9 Effect of Gr on temperature

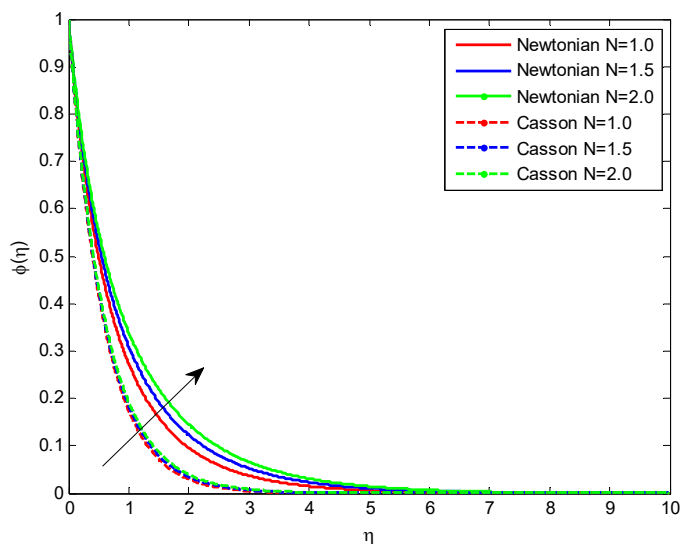


Fig. 7 Effect of N on Concentration

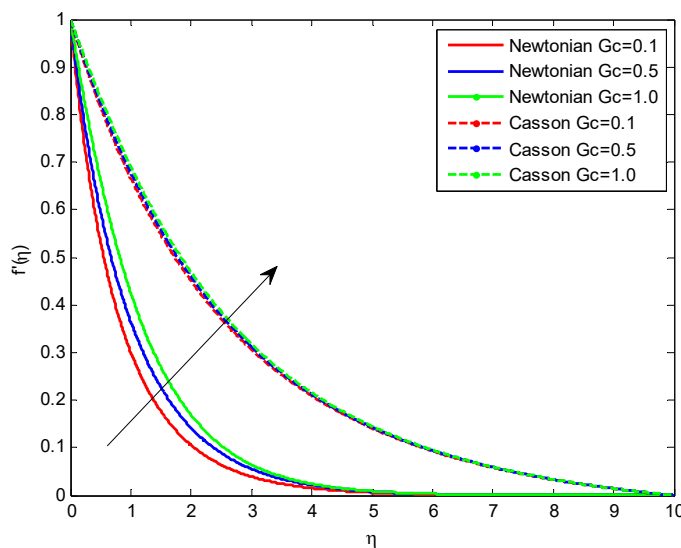


Fig. 10 Effect of Gc on velocity

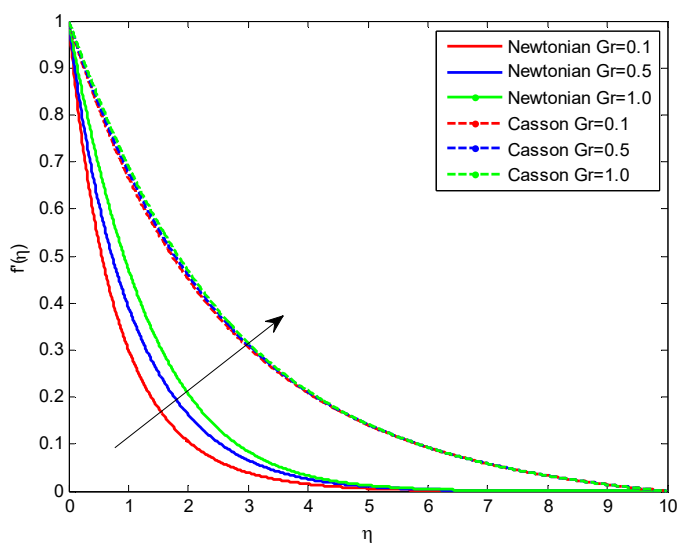


Fig. 8 Effect of Gr on Velocity

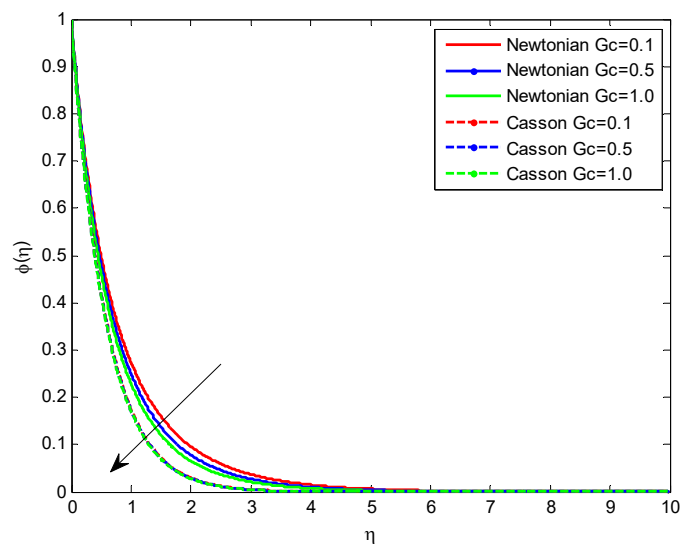


Fig. 11 Effect of Gc on Concentration

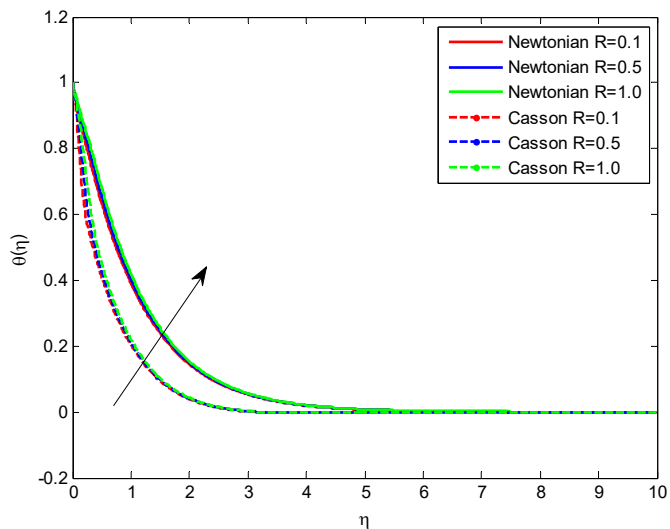


Fig. 12 Effect of R on temperature

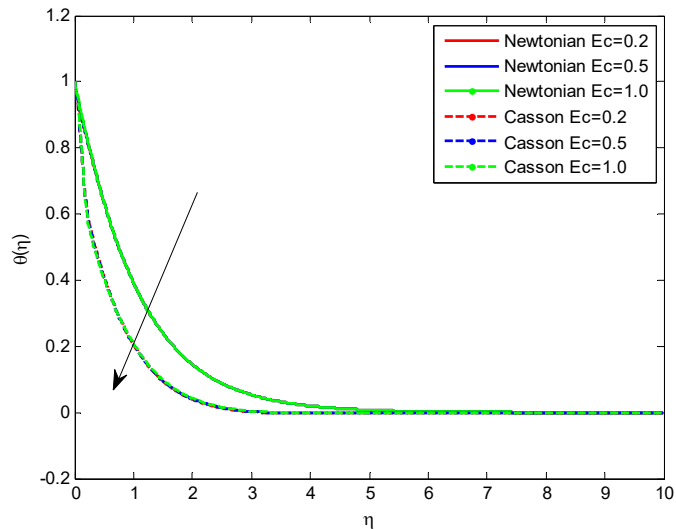


Fig. 15 Effect of Ec on Temperature

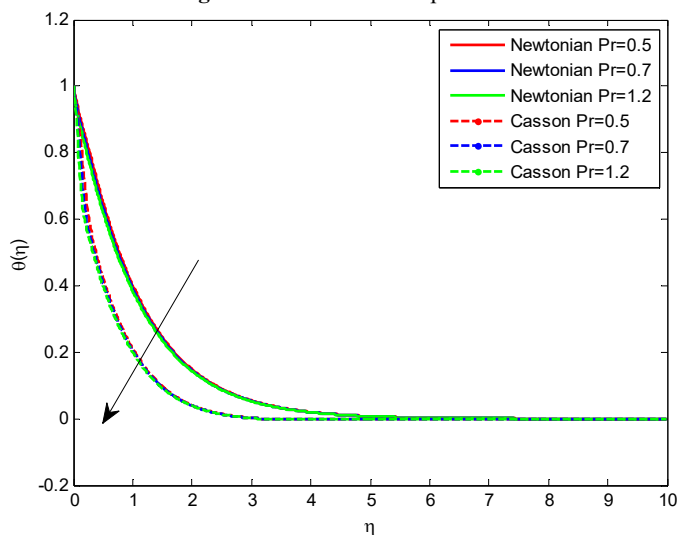


Fig. 13 Effect of Pr on Temperature

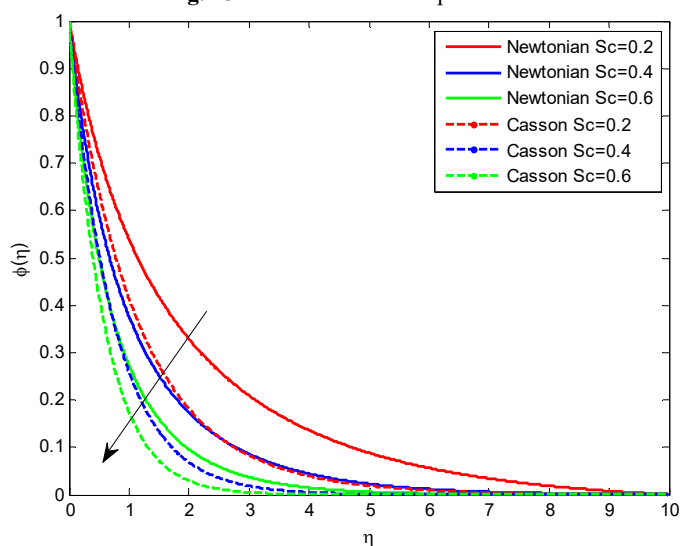


Fig. 16 Effect of Sc on concentration

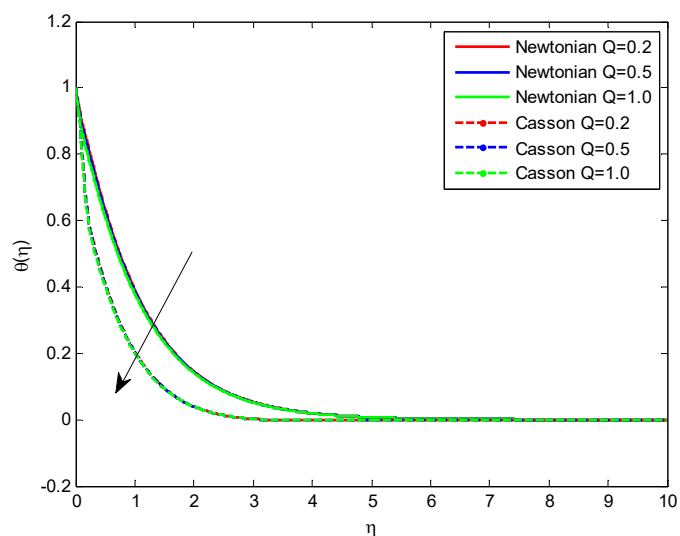


Fig. 14 Effect of Q on temperature

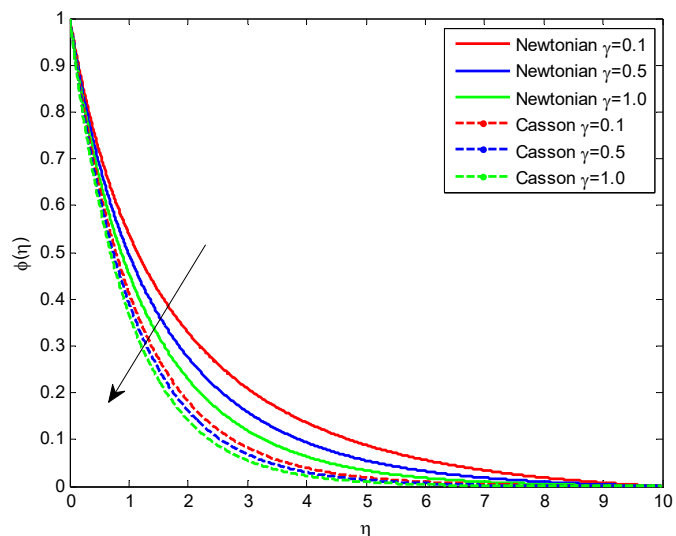


Fig. 17 Effect of γ on concentration

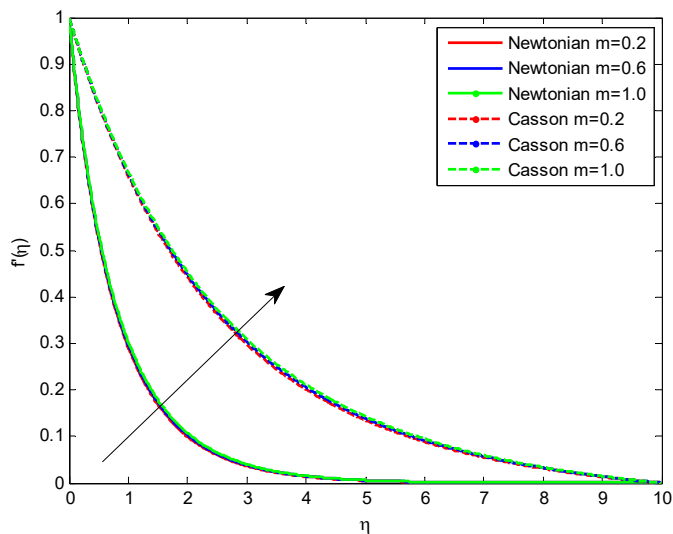


Fig. 18 Effect of m on velocity

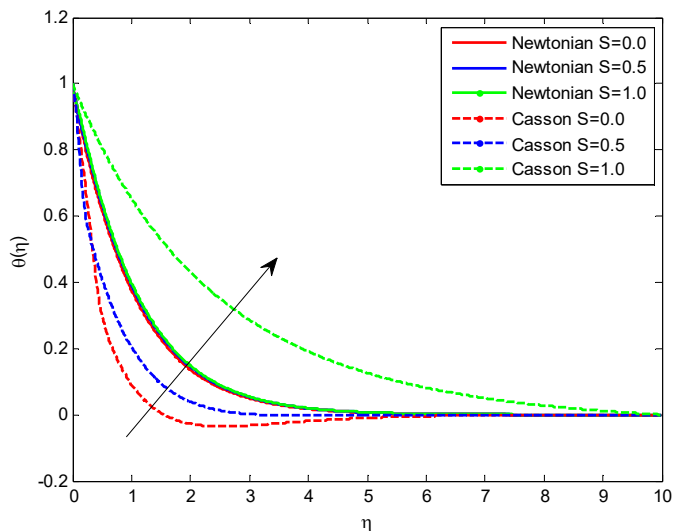


Fig. 21 Effect of S on temperature

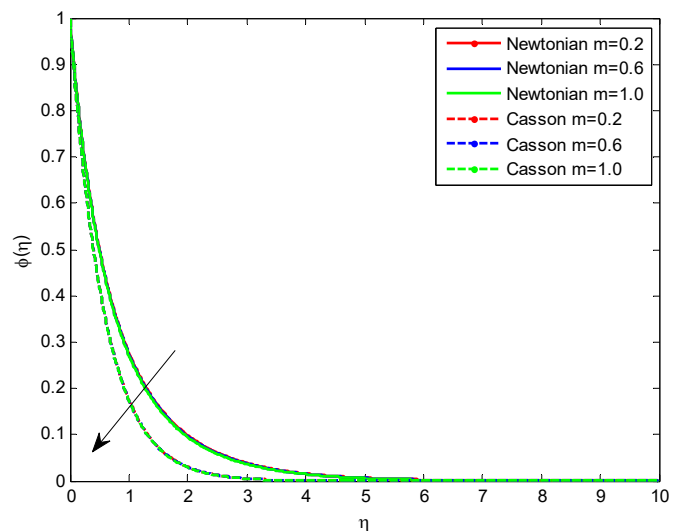


Fig. 19 Effect of m on Concentration

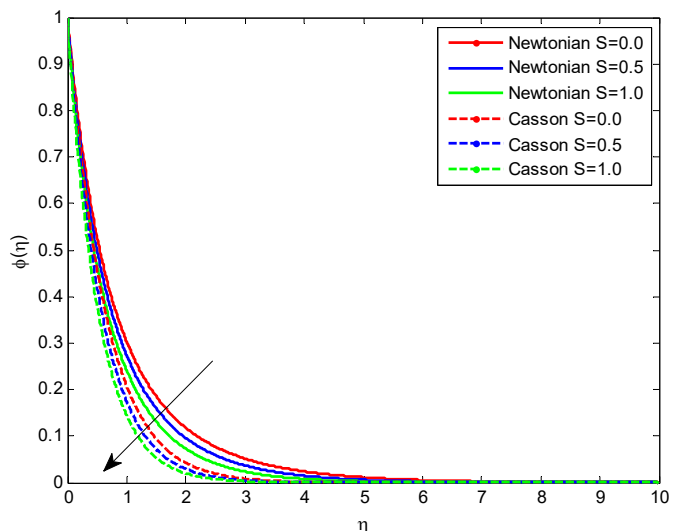


Fig. 22 Effect of S on Concentration

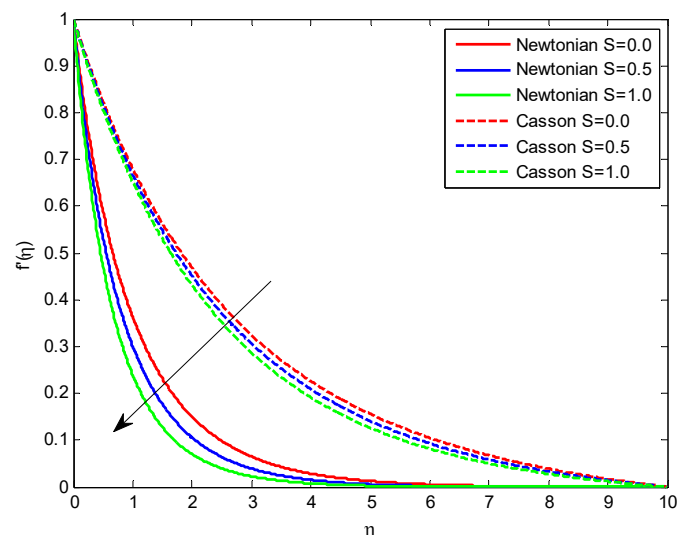


Fig. 20 Effect of S on velocity

Fig. 2, 3, 4 respectively indicates that with increase in the Hartmann number velocity decreases and temperature, concentration profiles increases due to an opposing force called Lorentz force. It is noticed that temperature plots rise adequately in case of Casson fluid when compared with Newtonian fluid. Fig. 5, 6, 7 respectively indicates that with increase in exponential parameter velocity, temperature and concentration profiles decreases because rise in exponential parameter causes reduction in momentum, thermal and concentration boundary layers. Fig. 8, 9 respectively indicates that with increase in thermal Grashof's number, raise in velocity profiles and decreasing tendency observed in temperature because developing buoyancy force suppress the value of contaminant concentration within the boundary layer regime normal to the barrier. Fig. 10, 11 indicates that with increase in concentration Grashof's number, raise in velocity profiles and fall in concentration profiles is observed. With increase in concentration Grashof's number momentum boundary layer thickness increases concentration boundary layer thickness decreases. Fig. 12 indicates that increase in Radiation parameter temperature enhancement is observed for both fluids. This happens due to the reason that raise in radiation heat energy with that effect temperature increases. Fig. 13 indicates that increase in Prandtl number temperature decreases for both fluids. For Large values of Prandtl number heat spreads slowly from surface when

compared to smaller values of Prandtl number. Fig. 14 indicates that increase in heat source parameter temperature diminishes for both the fluids due to decrease in thermal boundary layer thickness. Fig. 15 indicates that enhancement in Eckert number (Ec) raise in thermal conductivity of the fluid is observed so temperature of fluid increases. Fig.16 indicates that with increase in Schmidt number mass transfer increases so concentration profiles decreases. Fig. 17 indicates that increase in chemical reaction parameter, concentration profiles decreases. Fig. 18, 19 indicates that with increase in hall parameter, velocity increases and reverse trend is observed for temperature. Fig.20, 21, 22 indicates that increase in S fluid will come nearer to the surface which causes reduction in thermal, momentum and concentration boundary layer thickness diminishes so velocity and concentration profiles decreases.

To check the validity of the numerical method, results are compared with existing literature by calculating $-f''(0)$ for various values of magnetic field parameter (Hartmann number) by taking

$$Gr = Gc = S = 0.0, Rd = 1.0, N = 1.0, Pr = 0.7,$$

$$Sc = 0.7, Ec = 0.2, Q = 0.2, G = 0.1, B \rightarrow \infty$$

Table1 Comparison of $-f''(0)$

Ha	Present study	Ibrahim.et.al (HAM) (2020)	Kameswaran.et.al (RK Fehlberg) (2012)
0.0	1.281814	1.281803	1.281809
1.0	1.629147	1.629170	1.629178

By observing above table excellent correlation is observed with previous results for values of $-f''(0)$. On increasing Hartman number, substantial resistance in flow which causes raise in skin friction values. The influence of various parameters on the skin friction coefficient, Nusselt number, and Sherwood number for the Newtonian and Casson fluids is shown in Tables 2 and 3.

Table 2 Table of parameters skin friction coefficient, Nusselt number, Sherwood number in case of Newtonian fluid

N	Ha	Gr	Gc	S	Pr	R	Q	Ec	Sc	γ	J	m	$(1+\frac{1}{\beta})f''(0)$	$-(1+\frac{4R}{3})\theta'(0)$	$-\phi(0)$
1.5	0	0.1	0.1	0.5	0.7	0.1	0.2	0.2	0.6	0.1	0	0	-1.853711	1.56572	1.449699
	0.3												-1.873202	1.558491	1.445596
	0.8												-2.058748	1.477606	1.421723
1.5	0.5	0.2	0.1	0.5	0.7	0.1	0.2	0.2	0.6	0.1	0	0	-1.816384	1.579024	1.461124
	0.5												-1.565527	1.661807	1.515356
	1												-1.197801	1.762485	1.573135
1.5	0.5	0.1	0.2	0.5	0.7	0.1	0.2	0.2	0.6	0.1	0	0	-1.829514	1.582447	1.456583
	0.5												-1.612301	1.662566	1.501623
	1												-1.280476	1.753283	1.556699
1.5	0.5	0.1	0.1	0	0.7	0.1	0.2	0.2	0.6	0.1	0	0	-1.543743	1.248192	1.336602
	0.6												-1.990505	1.616101	1.460563
	1.2												-2.56068	2.059417	1.610409
1.5	0.5	0.1	0.1	0.5	0.3	0.1	0.2	0.2	0.6	0.1	0	0	-1.903033	0.866205	1.439758
	0.5												-1.905966	1.214185	1.438842
	1												-1.908353	2.026923	1.438156
1.5	0.5	0.1	0.1	0.5	0.7	0	0.2	0.2	0.6	0.1	0	0	-1.907713	1.496123	1.438335
	0.5												-1.905735	1.726055	1.438911
	1												-1.90387	1.931862	1.439489
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.1	0.2	0.6	0.1	0	0	-1.907028	1.497866	1.438517
	0.5												-1.90814	1.682265	1.438249
	1												-1.90951	1.906957	1.437917
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.2	0	0.6	0.1	0	0	-1.907395	1.636836	1.438447
	1												-1.906956	1.174491	1.438462
	2												-1.906517	0.712266	1.438477
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.2	0.2	0.4	0.1	0	0	-1.890318	1.555793	1.095974
	0.8												-1.918081	1.540782	1.705889
	1												-1.927983	1.536984	1.987027
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.2	0.2	0.6	0	0	0	-1.859435	1.543964	1.55865
	0.5												-1.871946	1.537716	1.707068
	1												-1.880958	1.534623	1.828975
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.2	0.2	0.6	0.1	0.1	0	-1.86252	1.531867	1.591498
	0.5												-1.862358	1.490644	1.591511
	1												-1.862156	1.439112	1.591526
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.2	0.2	0.6	0.1	0	0	-1.897509	1.522063	1.584614
	0.5												-1.879693	1.533472	1.588119
	1												-1.852591	1.546542	1.593463

Table-3 Table of parameters skin friction coefficient, Nusselt number, Sherwood number in case of Casson fluid.

N	Ha	Gr	Gc	S	Pr	R	Q	Ec	Sc	γ	J	m	$(1+\frac{1}{\beta})f''(0)$	$-(1+\frac{4R}{3})\theta'(0)$	$-\phi(0)$
1.5	0	0.1	0.1	0.5	0.7	0.1	0.2	0.2	0.6	0.1	0	0	-5.41424	1.853095	1.863675
	0.3												-5.46146	1.849093	1.862614
	0.8												-5.74174	1.824643	1.856298
1.5	0.5	0.2	0.1	0.5	0.7	0.1	0.2	0.2	0.6	0.1	0	0	-5.45567	1.846769	1.862275
	0.5												-5.19489	1.860468	1.866697
	1												-4.77694	1.881268	1.873588
1.5	0.5	0.1	0.2	0.5	0.7	0.1	0.2	0.2	0.6	0.1	0	0	-5.47823	1.844448	1.706777
	0.5												-5.21797	1.858093	1.710093
	0.8												-4.96048	1.871529	1.713391
1.5	0.5	0.1	0.1	0	0.7	0.1	0.2	0.2	0.6	0.1	0	0	-5.21825	1.915135	1.549382
	0.3												-5.63958	1.883	1.738069
	1												-6.11114	2.328931	1.938162
1.5	0.5	0.1	0.1	0.5	0.3	0.1	0.2	0.2	0.6	0.1	0	0	-5.53606	1.169879	1.860854
	0.5												-5.54173	1.525454	1.860779
	1												-5.54661	2.284788	1.860725
1.5	0.5	0.1	0.1	0.5	0.7	0	0.2	0.2	0.6	0.1	0	0	-5.54527	1.749458	1.860739
	0.5												-5.54127	2.184569	1.860784
	1												-5.53765	2.565606	1.860832
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.1	0.2	0.6	0.1	0	0	-5.54428	1.816144	1.86075
	0.5												-5.5449	1.918948	1.860741
	1												-5.54567	2.045509	1.86073
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.2	0	0.6	0.1	0	0	-3.55831	1.909817	1.629662
	0.5												-3.55758	1.187979	1.629666
	2												-3.55684	0.466352	1.62967
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.2	0.2	0.4	0.1	0	0	-5.51808	1.843645	1.348453
	0.8												-5.5492	1.841755	1.974509
	1												-5.55976	1.841257	2.249723
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.2	0.2	0.6	0	0	0	-5.53637	1.842327	1.686497
	0.5												-5.54139	1.842242	1.781922
	1												-5.54552	1.842129	1.869108
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.2	0.2	0.6	0.1	0.1	0	-5.53733	1.823603	1.706317
	0.5												-5.53674	1.748748	1.706326
	1												-5.53601	1.655172	1.706338
1.5	0.5	0.1	0.1	0.5	0.7	0.1	0.2	0.2	0.6	0.1	0	0	-5.664728	1.831206	1.703408
	0.5												-5.614168	1.835648	1.704563
	1												-5.537475	1.842316	1.706314

5. CONCLUSIONS

It is evident from the tables that

1. Raise in the Hartman number reduces the friction factor and the heat and mass transfer rates.
2. Increase in the radiation parameter, thermal Grashof number, and concentration Grashof number increases the skin friction coefficient and the heat and mass transfer rates.
3. The skin friction coefficient declines and the Nusselt number and the Sherwood number grow with increasing suction parameter.
4. As the Prandtl number and the heat source parameter increase, the heat transfer rate grows and the skin friction coefficient and mass transfer rate decrease.
5. Increase in the Eckert number enhances the skin friction coefficient and the mass transfer rate but depreciates the heat transfer rate.
6. As the chemical reaction parameter and Schmidt number rise, the mass transfer rate grows and the skin friction coefficient and the heat transfer rate decrease.
7. Increase in hall parameter, skin friction, heat transfer rate, and mass transfer rate increases.

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NOMENCLATURE

- Ha- Hartman's number
- N- Exponential Parameter
- Gr- Thermal Grashof number
- Gc- Concentration Grashof number
- R- Radiation parameter
- Pr- Prandtl number

Ec- Eckert number
Q- Heat generation parameter
Sc- Schmidt number
m- hall parameter
 ρ – density of the fluid
k- thermal conductivity of the fluid
 k_1 - chemical reaction rate
S- Suction parameter

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